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Research Paper

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ORAL IMPAC

Synergistic effect of oxygen species and vacancy for enhanced electrochemical $CO₂$ conversion to formate on indium oxide

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HIGHLIGHTS GRAPHICAL ABSTRACT

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*OCHO pathwa

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- Different amounts of oxygen species and vacancies were constructed on $In₂O₃$. • The *COOH pathway for $CO₂$ reduction to formate production on In_2O_3 was Productivity,
- confirmed. • 8.33% solar-to-formate and 10.11% solar-to-fuel were achieved when driven by photovoltaics.

ARTICLE INFO

Keywords: Electrocatalytic CO₂ reduction Formate In_2O_3 Oxygen species Oxygen vacancy

ABSTRACT

Indium-based oxides are promising electrocatalysts for producing formate via $CO₂$ reduction reaction, in which *OCHO is considered the key intermediate. Here, we identified that the *COOH pathway could be preferential to produce formate on In_2O_3 of In/In_2O_3 heterojunction due to the synergistic effect of oxygen species and vacancy. Specifically, *CO₂ and *COOH were observed on In₂O₃ and related to formate production by in situ Raman spectroscopy. The theoretical calculations further demonstrated that the energy barrier of the *COOH formation on In₂O₃ was decreased in the presence of oxygen vacancy, similar to or lower than that of the *OCHO formation on the In surface. As a result, a formate selectivity of over 90% was obtained on prepared In/In_2O_3 heterojunction with 343 \pm 7 mA cm⁻² partial current density. Furthermore, when using a Si-based photovoltaic as an energy supplier, 10.11% solar–to–fuel energy efficiency was achieved.

HCOOH HCOOH

1. Introduction

Converting $CO₂$ into fuels or chemical feedstocks is a promising strategy, which could alleviate the severity of the growing climate problem and recycle carbon resources $[1-5]$ $[1-5]$ $[1-5]$ $[1-5]$. The electrochemical $CO₂$ reduction reaction ($ECO₂RR$) proceeding at room temperature and pressure could utilize the electric energy generated from renewable energy like solar, wind, and tide, etc., which has become an attractive approach for highly efficient production [\[6](#page-6-1)–[8](#page-6-1)]. Among the reduction products such as methane [\[9](#page-6-2),[10](#page-6-3)], carbon monoxide (CO) [[11\]](#page-6-4), formate [\[12](#page-6-5)[,13\]](#page-6-6), ethanol [[14](#page-6-7),[15](#page-6-8)], ethylene [[16\]](#page-6-9), and oxygenates involving more carbon (C_{2+}) [\[17,](#page-6-10)[18\]](#page-6-11), formate has some advantages. The low thermodynamic potential and overpotential of formate production enable higher energy conversion efficiency, which has greatly gained researchers' interest. Besides, formate as a liquid product is easier to transport back and forth compared to CO production, which also involves two electrons [[19\]](#page-6-12).

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Recently, plenty of electrocatalysts have been explored to improve the activity and selectivity for $CO₂$ electroreduction and suppress the competing hydrogen evolution reduction (HER) [[20,](#page-7-0)[21\]](#page-7-1). Among them, $In₂O₃$, which is environmentally friendly and easy to be acquired, is one of the main electrocatalysts for formate production $[22]$ $[22]$. In/In₂O₃ heterojunction is the actual reacting electrocatalyst for the inevitable loss of O on In_2O_3 during the process of electrochemical CO_2 reaction [[23\]](#page-7-3). To promote formate selectivity and activity on $In/In₂O₃$ heterojunction, great efforts have been devoted, such as size and morphology designing [[24,](#page-7-4)[25\]](#page-7-5), defect engineering [[26,](#page-7-6)[27\]](#page-7-7), single-atom design [[28,](#page-7-8)[29\]](#page-7-9), doping introduction [[22,](#page-7-2)[30,](#page-7-10)[31\]](#page-7-11), and so on. However, only a few reports can achieve a current density over 300 mA cm^{-2} with Faradaic efficiency of formate (F E_{formate}) above 90% [\[32](#page-7-12)].

On In/In2O3 heterojunction, it is proved that In is the main reaction site to produce formate because of the electronic-rich surface [\[30](#page-7-10)]. At this pathway, $CO₂$ is firstly dissolved in the electrolyte to form bicarbonate and absorbed on In surface for hydrogenation reaction. This causes a slow reaction rate for low $CO₂$ solubility [\[24\]](#page-7-4). However, as the ratio of oxygen species on the surface of In/In_2O_3 heterojunction increases, the pathway of formate production might be changed. $CO₂$ could be absorbed by hydroxyl group on In_2O_3 or In surface. This allows formate production at wider overpotential and higher productivity, which means that the number of oxygen species on the surface of In/In₂O₃ heterojunction could change the CO_2 adsorption mode [\[23](#page-7-3)]. In addition, oxygen vacancies (O_v) are also considered an effective method to improve formate formation on In/In_2O_3 by improving CO_2 activation [[26](#page-7-6)[,33](#page-7-13)].

Here, we constructed $In/In₂O₃$ heterojunctions with different amounts of oxygen species and O_v to evaluate their electrochemical performance and explore the possible synergistic effect. In situ electrochemical surface-enhanced Raman spectroscopy (SERS) confirmed the *OCHO pathway for formate production on In sites of $In/In₂O₃$ heterojunction. Density-functional theory (DFT) calculations and SERS found that due to the synergistic effect of oxygen species and vacancy, the adsorption of *COOH was boosted and preferential to produce formate on In_2O_3 of In/In_2O_3 heterojunction. Subsequently, a Si-based photovoltaic and a gas diffusion electrode (GDE)-based electrolyzer were coupled using the optimized In/In₂O₃ heterojunction as a cathode.

2. Materials and methods

2.1. Synthesis of In_2O_3

The synthesis of prepared In_2O_3 is a typical hydrothermal method using a modified literature procedure (details in Supporting Information) [[34\]](#page-7-14). First, $In(OH)₃$ was prepared using InCl₃ as indium resource. After vigorously stirring for 30 min, urea was added. The resulting solution was moved into a Teflon–lined stainless–steel autoclave and maintained at 120 °C for 12 h. A kind of white substance was collected. Then, In_2O_3 was obtained after calcinated at 500 \degree C for 2 h in different atmosphere.

2.2. Characterization

Surface morphology and element characterization were performed by field emission scanning electron microscope (FE–SEM), and energy dispersive X-ray spectroscopy (EDS). Lattice spacing and valence characterization were determined by X-ray diffraction (XRD), X-ray photoelectron spectroscopy (XPS), transmission electron microscope (TEM), and electron paramagnetic resonance (EPR).

2.3. Electrode fabrication

In electrode was sputtered onto carbon paper under the Ar atmosphere using magnetron sputtering apparatus. Bulk $In₂O₃$ was used directly without any further treatment. Before electrode fabrication, the catalyst ink, which was composed of the prepared sample, Nafion, and isopropanol, was ultrasonic for sufficient dispersion. Catalyst loading was measured by weighing carbon paper before and after spray coating repeatedly. Before testing, the GDE was put still at room temperature in air overnight.

The anode for the photovoltaic-electrolyzer (PV-EC) system was fabricated by carrying out electrodeposition on Ni foam reported before [[35\]](#page-7-15). The electrolyte containing Ni(NO₃)₃⋅6H₂O and Fe(NO₃)₃⋅9H₂O was put in a breaker bathing in water to maintain 10° C. The deposition was carried out on nickel foam at -1 V (vs Ag/AgCl) for 300 s.

2.4. Electrochemical performance measurements

The customized flow cell electrolyzer with three electrodes was used to conduct property tests on catalysts. The prepared GDE, leak-free Ag/ AgCl, and platinum net acted as working electrode, reference electrode, and counter electrode, respectively. A piece of anion exchange membrane was put between catholyte chamber and anolyte chamber. An Auto-lab electrochemical workstation acted as energy supplier for all electrochemical measurements. Electrode potential was converted to reversible hydrogen electrode (RHE) considering the effect of pH and 80% iR compensation. The iR compensation was determined by electrochemical impedance spectroscopy measurement. During the process of CO2RR experiments, 1 M KOH solution was consistently pumped into the anolyte and catholyte chamber. The flow rate of $CO₂$ was maintained feeding continually into GDE by a mass flowmeter controller. Linear sweep voltammetry (LSV) was conducted at a scanning rate of 10 mV s⁻¹. The electrochemical active surface area was obtained under N_2 -purged 1 M KOH electrolyte. Electrochemical impendence spectroscopy was carried out from 100 KHz to 0.1 Hz.

2.5. In situ SERS measurements

The in situ SERS spectra were acquired using surface-enhanced Raman from Horiba, Lab RAM HR. The in situ Raman measurement was conducted using a customized electrocatalysis $CO₂$ reduction reactor, in which counter electrode was mounted far away from working electrode to avoid the effect of oxygen generating from counter electrode. To ensure the same condition, the three-electrodes system connected to an electrochemical workstation was just the same as the electrochemical performance test. Electrolyte was also pumped to chamber at the same flow rate by employing the same peristaltic tubing pump.

2.6. Computational method

The Vienna ab initio Simulation Package (VASP) was used to perform DFT calculations with plane-wave basis and periodic boundary conditions [\[36](#page-7-16),[37\]](#page-7-17). The Perdew–Burke–Ernzerhof (PBE) form of the generalized–gradient approximation (GGA) was chosen for electron exchange and correlation [\[38](#page-7-18)]. Three layers of In–O atoms were used for a small fluctuation within 0.1 eV and the fast-single electron step (Fig. S30). The lattice parameters of $In_2O_3(111)$ and $In(101)$ were presented in Fig. S31. The stable configuration of $In₂O₃–In$ was obtained by varying layer spacings. The solvation effects of aqueous electrolytes were considered by adding the solvation flag "LSOL=.TRUE., EB_k=78.4" (Table S4). The free energy change at the different potential was described by changing the applied potential in the CHE model (more details in Supporting Information) [[39,](#page-7-19)[40\]](#page-7-20).

3. Results and discussion

3.1. Introduction of different amount of O_v on In₂O₃

Flowerlike $In(OH)$ ₃ was chosen as the precursor for enhanced antireduction capacity (Supplementary information) [[23,](#page-7-3)[34\]](#page-7-14). Then, heat treatment was carried out at 500 °C in pure O_2 (In₂O₃–O) or air (In₂O₃–A) atmosphere [\(Fig. 1](#page-2-0)a). The phase transformation occurred slowly, and the

Fig. 1. Structural characterizations. (a) Schematic illustration of In₂O₃–A. (b) EPR of In₂O₃–A, In₂O₃–B, and In₂O₃–B, co. (c) O 1s XPS of In₂O₃–A and In₂O₃–B. (d) XRD of In₂O₃–A before and after in situ electroreduction. (e) TEM images of In/In₂O₃–A heterojunction.

white precursor $In(OH)₃$ would be converted to a faint yellow sample. As shown in Fig. S1, Raman peaks located at 130, 213, 309, 368, and 495 cm^{-1} belong to the characteristics of In₂O₃. It is suggested that the prepared In₂O₃ is a cubic phase with three main peaks of (222), (400), and (440) (Fig. S2). Morphology structure and elemental mapping show that In2O3 remains a flowerlike structure of a 9 μm diameter with uniform distribution of In and O elements (Figs. S3-S5 and Table S1). This leads to a surface area of 3.5 times larger than bulk In_2O_3 (In_2O_3-B) (Fig. S6). The lattice spacing of 0.29 nm is corresponding to the In_2O_3 (222) (Fig. S7). Importantly, due to the O_2 atmosphere, no signal was detected for In_2O_3 –O, as shown in [Fig. 1](#page-2-0)b. In comparison, In_2O_3 –A obtained in the air atmosphere has 50.29% O_v which is higher than that of In₂O₃–O with 47.87% but a little less than In_2O_3 -B with 50.41%, as shown in [Figs. 1](#page-2-0)c and S8.

3.2. Enhanced formate production due to the abundant oxygen species and O_v

The electrochemical performance was evaluated using a self-made three-electrode flow cell (Fig. S9). The electrode was fabricated by spraying the ink containing catalysts and Nafion onto a carbon paper substrate, which was served as the working electrode. $In/In₂O₃$ heterojunction was subsequently constructed through in situ electroreduction, which was carried out using cyclic voltammetry (CV) for two cycles (Fig. S10). After that, the electrochemical active surface area suggests that In/In₂O₃-A heterojunction has a 1.7 mF cm⁻² electrochemical double electric layer capacitance, which is much higher than 0.7 mF cm^{-2} of In/In₂O₃-B and 0.4 mF cm^{-2} of In. This implies that more electrochemical active sites exist on In/In₂O₃-A heterojunction (Fig. S11 and Table S2). XRD displays that the two peaks at 32.9 and 36.7 of In/ In₂O₃–A heterojunction are corresponding to In(101) and (110), respectively ([Figs. 1d](#page-2-0) and S12). [Figs. 1e](#page-2-0), S13, and S14 suggest the existence of In and In_2O_3 on the surface of the In/In_2O_3-A . Lower electron transfer resistance for In/In_2O_3-A is also achieved (Fig. S15). As the potential becomes more negative, In/In₂O₃-A heterojunction exhibits a significantly faster increase in current density, indicating $In/In₂O₃–A$ heterojunction possesses superior electrochemical activity, as shown in [Fig. 2](#page-3-0)a. To investigate and measure the Faradaic efficiency (FE) of products under different potentials, the ECO₂RR tests were carried out.

During the test, $In/In₂O₃–A heterojunction showed an almost linear$ relationship between potential and time, indicating its better stability compared to the other catalyst (Fig. S16). Formate is the main product generated by all samples at relatively positive potentials, with few H_2 and CO produced, as shown in [Figs. 2](#page-2-0)b and S17. When the potential turns more negative, In/In₂O₃-A heterojunction maintains high formate selectivity compared to In/In₂O₃-B, In/In₂O₃-O heterojunction and In, with a FE_{formate} of 90.5% at -1.29 V. Meanwhile, FE_{CO} and FE_{H₂} are 2.12% and 8%, respectively. The maximum $FE_{formate}$ of In/In₂O₃-A heterojunction is found to be 94.9% at -1.02 V. Additionally, a formate partial current density of 343 \pm 7 mA cm⁻² is obtained at -1.37 V, along with a formate yield of 6399 \pm 131 µmol cm⁻² h⁻¹, exceeding most previously reported $In/In₂O₃$ heterojunctions ([Figs. 2](#page-3-0)c, S18, and Table S7).

Few reports have carried out stability tests over 150 mA cm^{-2} for the gradual loss of oxygen element of In_2O_3 during the process of electrolysis, resulting in severe hydrogen evolution reaction [\[23](#page-7-3)[,24](#page-7-4)[,32](#page-7-12)]. Here, an 8-h stability test at 200 mA cm^{-2} of In/In₂O₃-A heterojunction is presented. The electrode potential exhibits only a slight change during the test, as shown in [Figs. 2](#page-3-0)d and S19. The FE_{formate} remains above 80% with a 160 mA cm^{-2} partial current density and a constant product yield is observed, indicating a stable electrode composition and three-phase interfaces. These metrics suggest that $In/In₂O₃–A$ heterojunction could be considered a promising electrocatalyst for its feasibility. Although a larger specific surface area may lead to higher current density, potential-dependent selectivity of formate demonstrates that specific surface area is not the main reason for improved selectivity at a wide potential range.

After in situ electroreduction by CV, a stable structure of In_2O_3 and In are constructed. The valence state of the indium element before and after the reaction is further verified. 444.5 eV and 452.1 eV are the reduced In⁰ $3d_{5/2}$ and $3d_{3/2}$ after comparison with In electrode, as shown in [Fig. 2e](#page-3-0). The binding energy of In³⁺ is considered higher than In⁰ [\[23](#page-7-3)[,41](#page-7-21)]. Therefore, 445.7 eV and 453.5 eV are corresponding to In^{3+} 3d_{5/2} and $3d_{3/2}$, respectively. It suggests that the ratio of In³⁺ on In/In₂O₃-A and In/In₂O₃–O heterojunction are 27.1% and 27.4%, respectively, higher than 5.2% of In/In₂O₃-B heterojunction ([Fig. 2](#page-3-0)f). This demonstrates that more oxygen species are present on the surface of In/In_2O_3-A and In/In2O3–O heterojunction. In addition, clear flowerlike structure and

Fig. 2. Electrochemical CO₂ reduction performance of In/In₂O₃-A, In/In₂O₃-B, In/In₂O₃-O, and In. (a) LSV. (b) Potential-dependent FE_{formate}. (c) Partial current densities of formate. (d) Stability test at 200 mA cm⁻² of In/In₂O₃-A. (e) In 3d XPS of three types of In/In₂O₃ heterojunction and In after reaction at -1.22 V vs RHE. (f) Schematic illustration of oxygen species on the surface of In/In_2O_3-A and In/In_2O_3-B .

Raman characteristic peaks after reaction at different current densities also show that In/In_2O_3 -A and In/In_2O_3 -O heterojunction have stronger anti-reduced capacity (Fig. S20). Meanwhile, Although In/In₂O₃-B has more O_v , which has been proven to enhance CO_2 reduction performance by suppressing HER, it cannot achieve high formate selectivity at a wide range of potential without enough oxygen species $[26]$ $[26]$. In/In₂O₃–O has enough oxygen species and could maintain selectivity to formate at higher overpotential, while it prefers for HER on oxygen species without O_v , which explains lower electrochemical activity. Consequently, considering improving the performance of formate production of In/In₂O₃–A heterojunction with abundant oxygen species and O_v (Fig. $S21$), we speculate that the O_v protected by abundant oxygen species might be the key structure for highly formate production on In/In₂O₃–A heterojunction.

3.3. The detection of intermediates and possible reaction pathways for formate production

The insight for improving catalytic performance of O_v protected by oxygen species was investigated. The in situ SERS test was implemented to identify possible intermediates of all samples in homemade Raman cell (Fig. $S22$). In/In₂O₃ heterojunction was constructed by CV. Each peak observed not caused by the changes in applied potential was analyzed first. Before immersing GDE into the electrolyte and applying potential, two main peaks were detected at 1350 cm^{-1} and 1615 cm^{-1} , which were the Eg and Dg of carbon paper by comparing the GDE with and without catalyst, as shown in Fig. S23 [\[32](#page-7-12)]. After introducing 1 M KOH electrolyte, a huge peak appeared after 3000 $\rm cm^{-1}$, attributed to adsorbed water on the surface of the catalyst. Another two new peaks were observed at 1065 cm⁻¹ and 1013 cm⁻¹, corresponding to the vibration of potassium carbonate when introducing $CO₂$ to the back of GDE [\[42](#page-7-22)]. Open circuit potential was then applied to the electrode, without any significant change for all three electrodes. Electrode potential was applied at the range of -0.32 V to -1.52 V vs RHE with the recording of signals. Between 900 cm^{-1} and 1800 cm^{-1} , another three new peaks appeared at 1155 cm⁻¹, 1380 cm⁻¹, and 1530 cm⁻¹ on In/In₂O₃ heterojunction, as shown in [Figs. 3](#page-4-0)a and b, and S24. Comparing the computed value (Fig. S25) and previously reported works [\[42](#page-7-22)–[44](#page-7-22)], we concluded that the

first and last peaks were the unprotonated intermediates, which were the C=O stretching vibration of adsorbed carbonate (v_s COO⁻) and the C-O stretching vibration mode (v_{as} COO⁻), respectively [[42,](#page-7-22)[43,](#page-7-23)[45,](#page-7-24)[46\]](#page-7-25). The second peak was protonated intermediates, which was the C–O stretching of *COOH intermediate ([Fig. 3](#page-4-0)c, in red dashed lines) [\[42](#page-7-22)[,43](#page-7-23)[,47](#page-7-26)]. As for $In/In₂O₃$ -O with more oxygen species but less vacancy has weak signal of $*$ COOH. In/In₂O₃-B with less oxygen species but more vacancy has a higher signal. Furthermore, In/In_2O_3-A exhibited the highest *COOH Raman signal for the more oxygen species and vacancy [\(Fig. 3c](#page-4-0), the first arrow). Between 2700 cm^{-1} and 3200 cm^{-1} , a new peak of the ^C–H bond in *OCHO on all electrodes was confirmed located at 2814 cm^{-1} [[42\]](#page-7-22).

Next, the possible reaction pathways of enhanced formate production on In/In_2O_3-A heterojunction are further analyzed. It is clear that the reaction intermediate on In for $CO₂$ reduction to formate only involves *OCHO. In/In₂O₃-A and In/In₂O₃-O have same ratio of oxygen species and In⁰ on the surface and nearly the same intensity of $*$ OCHO, as shown in Fig. S26. Meanwhile, In/In₂O₃-B has higher ratio of In⁰ and higher intensity of *OCHO, which implies that *OCHO might only exist on In^0 . $*CO₂$ and $*COOH$ just existed on the In₂O₃ surface of In/In₂O₃. $*CO₂$ was rich on the surface of In/In_2O_3-A due to the abundant oxygen species and O_v (Figs. S27 and S28). Furthermore, the Raman signal of *COOH on In/ In₂O₃–A was higher than that on In/In₂O₃–B and In/In₂O₃–O [\(Fig. 3c](#page-4-0)). It means that the CO_2 -rich environment on In/In₂O₃-A influenced the reaction pathway involving *COOH. Some reports think that *COOH is the reaction intermediate to produce CO, while HER rather than CO production is the main competing reaction here (Fig. S29) [[48,](#page-7-27)[49\]](#page-7-28). Therefore, the $*CO₂$ and $*COOH$ might be the reaction intermediates for formate production, which has been reported on Sn-based electrocatalysts [[33,](#page-7-13)[47](#page-7-26)[,50](#page-7-29)–[52\]](#page-7-29).

3.4. The energy barrier analysis of the possible reaction pathway for formate production

To verify the assumed reacting pathways, DFT was used to analyze the energy barrier of the possible reaction pathway. On the In_2O_3 surface, we found two types of $*CO_2$ configurations, with the C–O bond parallel to the surface or V-shaped symmetric adsorption. The hydrogenation of

Fig. 3. The potential-dependent *in situ* SERS spectra. (a) In. (b) In/In₂O₃–A between 900–1800 cm^{–1} and 2700–3200 cm^{–1}. *OCHO was observed on both catalysts, while v_s COO⁻, v_{as} COO⁻, and *COOH were only observed on In/In₂O₃ heterojunction. (c) In situ Raman signal of *COOH at three types of In/In₂O₃ and In.

*CO2 to form *COOH or *OCHO intermediates can be achieved by adding H^{$+$} to O or C atoms. The influence of two types of $^{\star}CO_{2}$ named 1 and 2 on the reaction pathway was analyzed by removing the surface O that bonds with $*CO₂$ (Fig. S32).

*CO2 adsorption is present and related to crystal facets as well as catalysts during the reaction process $[47,53]$ $[47,53]$ $[47,53]$. DFT results show $CO₂$ cannot form a stable bond with In surface, consistent with Raman signal. On the surface of In_2O_3 , *HCOOH is easier for direct desorption. On the In surface [\(Fig. 4](#page-5-0)a), as the *OCHO has lower Gibbs free energy than *COOH, formate produced from the *OCHO pathway is preferred, with an energy barrier of 0.656 eV, lower than 0.919 eV via the *COOH pathway. The presence of surface O on In_2O_3 can facilitate the adsorption of CO2 and *COOH intermediates compared to In. However, the stronger adsorption of *COOH makes desorption more challenging (Fig. S33 and Table S3). After the introduction of O_v (In₂O₃–O_v), although the *OCHO is the minimum energy pathway and more stable than *COOH, its desorption is hard, leading to surface accumulation and poisoning of active sites (consistent with the gradual enhancement phenomenon of *OCHO intensity on in situ Raman spectroscopy in Fig. S26b). When considering the limiting potential at which each step is thermodynamically favorable, the limiting potential for the *COOH pathway is similar to (0.646 eV) or even lower (0.478 eV) than the *OCHO pathway for formate production on the In surface. These variations suggest that the electroreduction of CO2 to formate through the *COOH pathway on the $In_2O_3-O_v$ surface is also allowed. When applying the corresponding

potential to the electrode, such as -0.656 V, -1.009 V, and -1.41 V vs RHE (based on Table S3), the pathway in which every step is exothermic will open, following the order about the lowest limiting potential. For example, at -0.656 V vs RHE, the *COOH pathway is thermodynamically favorable in In_2O_3 -2- O_v while the *OCHO pathway is blocked due to the higher desorption barrier (Fig. S34). At -1.009 V vs RHE, $*$ COOH and *OCHO pathways are both favorable in $In_2O_3-2-O_v$ and In surface (Fig. S35). At -1.41 V vs RHE, *COOH and *OCHO pathways are both thermodynamically favorable in $In_2O_3-1-O_v$ and $In_2O_3-2-O_v$ surface (Fig. S36). More details are discussed in Supplementary information.

The reason for the enhanced adsorption capacity of *COOH compared to the In was explored by Crystal orbital Hamilton population (COHP) analysis and Bader charge [[54](#page-7-31)–[56\]](#page-7-31). Due to the existence of oxygen species, In atom has a higher positive charge on the In_2O_3 surface than on the pure In, with the Bader charge increased from 0.32 to 1.76, as shown in [Figs. 4](#page-5-0)b and c, and S37. The more electropositive In will have a stronger binding ability to the O atom in *COOH. On both $In_2O_3-O_v$ and In surfaces, the integrated COHP (–ICOHP) of the C–In bond remains around 3.4, indicating similar C–In bond adsorption strength. However, the –ICOHP of the C–O bond increases from 1.58 on the In surface to 3.26 on the $In_2O_3-O_v$ surface. The above results indicate that the enhanced adsorption capacity of *COOH on the $In_2O_3-O_v$ surface mainly comes from its stronger O–In bond interaction. In conclusion, the *COOH pathway on $In_2O_3-O_v$, as well as the *OCHO pathway on In/In_2O_3-Ov , explains the more efficient formate production on In/In_2O_3-A [\(Fig. 4](#page-5-0)d).

Fig. 4. The evaluation of possible reaction pathway. (a) Gibbs free-energy diagrams of CO₂ reduction to formate on In and In₂O₃-O_v through *COOH (upper panel) and *OCHO (lower panel) pathways, respectively at 0 V vs RHE. (b) The –ICOHP analysis of C–O bond and C–In bond on $In_2O_3-O_V$ and In surfaces. (c) The results of calculated charge density among In and O atoms. (d) Schematic illustration of two types of reaction pathways on $In_2O_3-O_v$ and $In/In_2O_3-O_v$ surfaces, respectively.

Fig. 5. The results of the solar-driven formate production. (a) Schematic illustration of PV-driven CO₂RR system. (b) The current-potential (j-V_{cell}) curve of Si-based solar cells at 476 W m⁻² illuminations and CO₂RR electrolyzer. (c) Radiation intensity, photocurrent and partial current density of formate, solar to fuels and formate, FEformate, and yield of formate distribution under natural light conditions.

3.5. Solar-driven formate production

The feasibility of formate production driven by sustainable energy was conducted by coupling the GDE-based $CO₂RR$ electrolyzer with a Sibased solar cell to power $CO₂$ reduction using solar energy ([Figs. 5a](#page-5-1) and S38). In this system, the prepared $In/In₂O₃–A$ heterojunction served as the cathode. The Ni/Fe LDH was successfully prepared and used as the anode due to lower overpotential than Pt (Figs. S39–S41) [\[35](#page-7-15)]. The electrolyzer was assembled as tested above. Eight commercial Si solar cell in tandem with 24.8 cm^{-2} total illumination areas was used as an electric supplier. The PV cell was fixed on an auto-tracking model to make sure that the sunlight irradiated vertically onto the PV cell at all times [\[57](#page-7-32)]. As shown in [Fig. 5c](#page-5-1), after one natural day of 8 h, we got a maximum of 10.11% solar-to-fuel and 8.33% solar-to-formate energy conversion efficiency, exceeding most reported Si-based PV-EC (Table S5). Meanwhile, selectivity of formate remains over 88% with a maximum partial current density of 98 mA $\rm cm^{-2}.$ The productivity of formate grows smoothly to 11.15 mmol one day (Table S6). The best energy efficiency appears at 4:00 pm for the appropriate couple with 22.74% efficiency for the PV ([Figs. 5b](#page-5-1) and S42).

4. Conclusions

In summary, we first prepared three types of In/In₂O₃ heterojunction with different amount of oxygen species and O_v . After electrochemical tests, In/In₂O₃ heterojunction containing more oxygen species as well as O_v had higher formate production activity than that with only one feature. This indicated the synergistic effect between the oxygen species and O_v . The in situ SERS confirmed two types of unprotonated *CO_2 and *COOH on the $In_2O_3-O_v$ surface, while the protonated *OCHO existed on In surface. DFT calculation results showed that $CO₂$ could not form a stable bond with In atom, consistent with in situ SERS. Although $^{\ast}CO_{2}$ could be achieved on In_2O_3 surface, the formate production was inhibited for the high*COOH formation energy. Introduced O_v greatly decreased the energy barrier of *COOH formation on the In₂O₃ surface, which was similar to or lower than that of the *OCHO pathway on In surface. In comparison, formate production via *OCHO on the $In_2O_3-O_V$ surface was blocked for the higher energy barrier than *COOH. This leads to formate production via the *COOH pathway on the $In_2O_3-O_v$ surface, as well as the *OCHO pathway on the In surface. Furthermore, the prepared $In/In₂O₃$ heterojunction exhibits a formate selectivity over 80% under a wide potential range of -0.69 to -1.37 V vs RHE. Particularly, a formate partial current density of 343 \pm 7 mA $\rm cm^{-2}$ was achieved, exceeding previously reported In/In₂O₃ heterojunction. Under this fundamental understanding, a Si-based photovoltaic and GDE-based electrolyzer were coupled using the prepared In/In₂O₃ heterojunction as the cathode. Under natural light irradiation, 10.11% solar-to-fuel and 8.33% solar-to-formate energy efficiency were achieved, surpassing most reported Si-based PV-EC. This work provides a new strategy for collaborative utilization of oxygen species and O_v to modulate the reaction pathway and enhance electrocatalytic $CO₂$ reduction for formate production and practical applications driven by sustainable energy.

Author contributions

Tengfei Ma: Writing – original draft, Formal analysis, Data curation, Conceptualization. Zihao Jiao: Formal analysis, Conceptualization. Haoran Qiu: Methodology, Data curation. Feng Wang: Methodology, Formal analysis. Ya Liu: Writing – review & editing, Supervision, Formal analysis, Conceptualization. Liejin Guo: Writing – review $\&$ editing, Resources, Project administration, Conceptualization.

Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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Appendix A. Supplementary data

Supplementary data to this article can be found online at [https://do](https://doi.org/10.1016/j.esci.2024.100246) [i.org/10.1016/j.esci.2024.100246.](https://doi.org/10.1016/j.esci.2024.100246)

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